Original Research

# Characterization and Optimization of Photocatalytic Activity of Sol Gel-Synthesized TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub> through Degradation of Synthetic Textile Effluent by UV Lamp-Assisted Experimental Setup

# Tayyaba Muhammad Akram<sup>1,2</sup>\*, Nasir Ahmad<sup>3</sup>, Irfan Ahmed Shaikh<sup>1</sup>

<sup>1</sup>College of Earth and Environmental Sciences, University of the Punjab, Lahore, Pakistan <sup>2</sup>Department of Science Education (IER), University of the Punjab, Lahore, Pakistan <sup>3</sup>Institute of Geology, University of the Punjab, Lahore, Pakistan

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## Abstract

The textile industry is one of the largest producers of harmful effluent, and this has become a serious threat to the environment when disposed of into water bodies, which may lead to high pollution risk - especially in developing countries. There are several treatment methods ranging from conventional to advanced for treating textile effluent before disposal in the environment. Photocatalytic oxidation (AOPs) is the most sophisticated process among all other advanced oxidation processes. In this study, TiO, and Ag-doped TiO2 were used for the photcatalytic degradation of synthetic textile effluent. TiO, and Ag-doped TiO, catalyst were synthesized through two routes of sol-gel method (M1 and M2 reported in our previous study) for mobilized and immobilized utilization purposes [1], and characterization of the catalysts was carried out through X-ray diffrectrometric analysis. XRD patterns showed that catalysts synthesized by both routs of sol-gel method were initially found in amorphous form as no peak appeared in an X-ray diffractrogram at 0°C calcination (catalyst without calcinations), whereas with an increase of temperature the amorphous form of catalyst turned into crystalline. Results showed that TiO, synthesized by the sol-gel route showed anatase phase at 350°C, and peaks kept growing until 550°C. Furthermore, at 650-750°C anatase and rutile co-exist, while in Ag-doped TiO,, anatase appeared at 350-450°C and at 550°C anatase phase/silver co-existed, whereas at 650-750°C anatse-silver-rutile co-existed. An X-ray diffractrogram showed that catalyst synthesized through the 2<sup>nd</sup> sol-gel route also possessed an amorphous nature at 350°C and peaks of anatase phase of TiO, appeared at 450°C and kept growing sharper as temperature increased from 450-750°C, whereas anatase peaks detected at 350°C in Ag-TiO<sub>2</sub>, and anatase-silver co-existed at 450°C and 550°C. Hence, anatase disappeared

<sup>\*</sup>e-mail: tmabpu@hotmail.com

and only silver metal peaks remained at 650-750°C. Degradation and decolorization results revealed that optimum photocatalytic activity was achieved by catalysts calcinated at 550°C as 91.96% degradation (COD removal %) with Ag-doped TiO<sub>2</sub> immobilized catalyst, and 99.57% decolorization (colour removal percentage) was achieved with Ag-doped TiO<sub>2</sub> mobilized catalyst on 60 min treatment of synthetic textile effluent (Remazol red RGB: 10 ppm concentration, pH3). Results showed that Ag-doped TiO<sub>2</sub> developed anatase crystalline phase at 550°C that favored degradation and decolourization. The order of catalyst calcination at 550°C with respect to degradation was found as Ag-TiO<sub>2</sub> (immobilized) > Ag-TiO<sub>2</sub> (mobilized) > TiO<sub>2</sub> (immobilized) > TiO<sub>2</sub> (immobilized) > TiO<sub>2</sub> (mobilized) = TiO<sub>2</sub> (mobi

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## Introduction

The textile industry is one of the largest effluentproducing sectors. Textile effluent generally contains a huge amount of dyes and chemicals that are considered to be toxic, carcinogenic, and harmful for the environment when disposed of in water bodies [2-8]. Advanced oxidation processes (AOPs) have been proven to be very effective for removing organic and inorganic pollutants, color, COD, and toxicity from textile effluent [9, 10]. Among AOPs, heterogeneous TiO<sub>2</sub> photocatalysis is the most sophisticated technology for oxidation of dyes and textile wastewater [11-18]. Titanium dioxide occurs in nature in wellknown minerals such as rutile (tetragonal), anatase (tetragonal), and brookite (orthorhombic). Each phase of catalysis exhibits different physical properties, which are determined by their structural, chemical, and optoelectronic properties, which means that catalytic activity strongly depends upon its size, crystallinity, and shape [19-24]. These properties are controlled by the preparation conditions of the catalyst such as calcination temperature, calcination time, pH of the medium, and concentration (ratio of titanium tetrabuta oxide, water, and solvent) [25-28]. It is a well-established fact that calcination time and concentration ratio have no significant effect on the catalyst synthesis, whereas pH and calcination temperatures of the medium play vital roles in the anatase, rutile, and brokite crystal phase transformation and controlling the size of the crystallite, which effects the efficiency of the catalyst in degradation and decolorization of the textile effluent [29-34]. Calcination is a common treatment used to improve the crystallinity of TiO, powders and it was found that phase transformation from amorphous to crystalline anatase occurred at temperatures above 350°C [35, 36]. Synthesis of the catalyst sees two simultaneous reactions (hydrolysis and condensation) taking place that affect the crystallite size and the formation of the crystal phase. These reactions are sensitive to pH of the reaction medium. Acidic pH is used to restrain hydrolysis, while alkali can accelerate

hydrolysis during reaction. Acidic medium is favorable for the synthesis of small crystallite, more active sites, and the formation of the anatase phase [24, 37, 38]. The effect of pH on crystallite size is a well-established fact. When the pH value is below 7 the size of crystallites are almost small and remain constant, which means acidic medium restrains crystallite growth, whereas pH value beyond 7 indicates that a total alkali environment would enhance crystallite size growth, which reduces the active site of the catalyst that is not favorable for the efficient photocatalytic oxidation of the pollutant. Smaller crystallite size and high active sites results in higher efficiency in the photodecomposition of the pollutants [30, 39-41].

In this study, the main focus was to synthesis catalysts ( $TiO_2$  and Ag-doped  $TiO_2$ ) to calcinate at different temperatures, to characterize in order to determine crystalline phase and structure, and to evaluate photocatalytic activity (performance) by COD removal and colour removal percentages.

#### **Material and Methods**

#### Synthesis and Doping Process of the Catalysts

TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub> catalyst was synthesized through two routes of sol-gel method M1 and M2 for mobilized and immobilized application, respectively (these routes are reported in our previous research paper [1]). The synthesis of the catalyst and doping process was carried out by following a modified sol-gel method and then calcinated at 350°C, 450°C, 550°C, 650°C, and 750°C [1]. Substrate was prepared and coating the thin film catalyst was carried out by standard slurry coating method [1, 42].

#### Material and Chemicals

Titanium tetraisopropaoxide (97%), acitic acid (99.7%), silver nitrate (99%), nitric acid, ethanol, deionized water, and dental material.

#### Equipment and Instrumentation

A magnetic stirrer (0-1400 rpm) for continuous mixing of the effluent, analytical balance (Sartorius, BL 210S), oven (maximum range 250°C), furnace. Characterization of the catalyst calcinated at 350°C, 450°C, 550°C, 650°C, and 750°C was carried out by a Rigaku X-ray powder diffractometer (D-maxIIA, Rigaku, Japan), photocatalytic degradation was carried out in a double-walled rectangular box reactor (double-walled horizontal glass reactor [1].

#### Methodology

In this study, pH of the medium was kept acidic at 2 during the synthesis of the catalyst, which is favorable for small crystal size by preventing hydrolysis that restrains large crystal growth. TiO, was used alone as well as being doped with Ag metal to reduce the gape of valance and conduction band, and also to control the electron-hole recombination rate. Catalysts were then calcinated at 350°C, 450°C, 550°C, 650°C, and 750°C to obtain desired anatase phase of TiO, to improve the crystallinity in order to enhance performance of the catalysts [28, 35, 43-45]. Performance of the catalyst was evaluated by degradation (COD removal percentage) and decolorization (colour removal percentage) of synthetic textile effluent (Remazol red RGB dye containing 10 ppm concentration, pH3) through mobilized and immobilized TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub> under UV (400W) irradiation for 60 mins. For this purpose we used a double-walled rectangular box reactor (double walled horizontal glass reactor) [1].

#### **Results and Discussion**

#### Characterization of the Catalysts

TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub> catalysts were characterized by X-ray diffractrometer (D-maxIIA, Rigaku, Japan) for determining the effect of calcination temperature on catalyst properties, such as crystalline phase, structure/ lattice, crystal size (nm), percent crystal, and percent amorphous ratio of the catalysts [33, 46-48]. Fig. 1 through 4 show the patterns of X-ray diffraction of TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub>, and Tables 1 through 4 summarize the X-ray diffractromtric data.

Figs 1 and 2 show the patterns of X-ray diffraction of  $\text{TiO}_2$  and Ag-doped  $\text{TiO}_2$  (synthesized by M1 route of sol gel) used in mobilized applications.  $\text{TiO}_2$  and Ag doped  $\text{TiO}_2$  were coded as M1A and M1B (neither pulverized nor calcinated), respectively. Furthermore, M1A1 and M1B1 (pulverized but not calcinated), M1A2 and M1B2 (calcinated at 350°C), M1A3 and M1B3 (calcinated at 450°C), M1A4 and M1B4 (calcinated at 550°C), M1A5 and M1B5 (calcinated at 650°C), and M1A6 and M1B6 (calcinated at 750°C). It appears from figures 1 and 2 that in catalyst M1A1 and M1B1 (pulverized but not calcinated) peaks corresponding to anatase are absent, which implies that pure and doped titania are in amorphous form and showed lowest catalytic performance (Fig. 5). Hence, titania catalyst (pure TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub>) were calcinated for obtaining desired anatase crystal structure having high photocatalytic activity [49]. Pure TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub> catalysts coded as M1A2 and M1B2, M1A3 and M1B3, M1A4 and M1B4, M1A5 and M1B5, and M1A6 and M1B6 were calcinated at 350°C, 450°C, 550°C, 650°C, and 750°C, respectively.

Figs 1-4 demonstrated that diffraction peaks appearing at  $2\theta$  value correspond to the crystal phase of the catalyst (TiO<sub>2</sub> and Ag-doped TiO<sub>2</sub>). The peaks



Fig. 1. X-ray diffractrograms of TiO<sub>2</sub> catalyst: 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750 °C temperatures (TiO<sub>2</sub> catalyst synthesized through Ist sol gel route and used as mobilized form, A = anatase, R = rutile).



Fig. .2. X-ray diffractrograms of Ag doped  $\text{TiO}_2$  catalyst: 0°C (without calcinations), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures (Ag-TiO<sub>2</sub> catalyst synthesized through Ist sol gel route and used as mobilized form, A = Anatase, S = Silver).

of the XRD graphs shown in figures are in agreement with findings reported in the literature, and very well matched with the profile provided by the joint committee on powder diffraction standards.

However, X-ray diffractogram of M1A2, M1A3, and M1A4 (Fig. 1) exhibited strong diffraction corresponding peaks of titanium oxide matched with JCPDS files PDF: 04-0477 ( $2\theta = 25.354$ , 37.785, 38.507, 53. 922, 55.116, and 62.728), PDF: 86-1157 (25.322, 37.863, 48.064, 53.975, 55.094, and 62.756), and PDF: 86-1157 (25.322, 37.863, 48.064, 53.975, 55.094, 62.756,



Fig. 3 X-ray diffractrograms of TiO<sub>2</sub> catalyst: 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures (TiO<sub>2</sub> catalyst synthesized through second sol gel route and used as immobilized, A = anatase).

70.330, and 75.141), and crystallite phase was confirmed as anatase and lattice structure was tetragonal. The crystal size for the anatase was 9.34 nm, 14.83 nm, and 18.01 nm, and the percent crystal and percent amorphous ratios were 60.4:39.6, 58.8:41.2, and 68.9:31.1, respectively. X-ray diffractrograms illustrate that the anatase phase of TiO<sub>2</sub> is dominating and became sharper as calcination temperatures increased to 550°C, but going to 650-750°C rutile phase appeared and few anatase peaks started to degrade/disappear.

X-ray diffractogram of M1B2 calcinated at 350°C (Fig. 2) indicates corresponding peaks of titanium oxide matched with JCPDS profile PDF: 78-2486



Fig. 4. X-ray diffractrograms of Ag doped TiO<sub>2</sub> catalyst: 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures (Ag-TiO<sub>2</sub> catalyst synthesized through second sol gel route and used as immobilized, A = Anatase, S = Silver).

 $(2\theta = 25.307, 37.79, 48.043, 55.068, 62.689, 70.298, and 75.05)$ , crystallite phase was anatase, lattice structure was tetragonal, crystal size was 13.82 nm, and the percent crystal and percent amorphous ratio was found to be 50.87:49.24. Catalyst M1B3 calcinated at 450°C (Fig. 2) showed corresponding peaks of titanium oxide matched with JCPDS profile PDF: 86-1157 ( $2\theta = 25.322$ , 37.863, 48.064, 53.975, 62.756, 68.870, and 75.141), crystallite phase of composite of anatase, lattice structure of tetragonal. Crystal size of the anatase was found to be 14.6 nm and percent crystal and percent amorphous ratio was found to be

49.7:50.3. Whereas, catalyst M1B4 calcinated at 550°C (Fig. 2) possessed corresponding peaks of titanium oxide/silver matched with JCPDS profile PDF: 86-1157 ( $2\theta = 25.322$ , 48.062, 55.094, 62.756, 68.870, and 76.08) PDF: 87-0720 (38.201, 44.402, 64.602, and 77.600), anatase/silver crystals were identified in the catalyst, and latice structure was composite of tetragonal/cubic, crystal size was 23.19 nm, as well as percent crystal and percent amorphous ratio was found to be 59.5:40.5. Silver and TiO<sub>2</sub> composite crystal structure appeared at 550°C and its catalytic performance also increased (Fig. 5) due to the electron scavenging property of Ag and the reducing band gape energy of TiO<sub>2</sub>.

Catalysts M1A5 and M1A6 calcinated at 650°C and 750°C (Fig. 1) revealed that as temperature increased to more than 550°C, the corresponding peaks of titanium oxide crystalites turned to rutile/anatase composite phase and matched with JCPDS profile PDF: 86-1156  $(2\theta = 25.335, 37.809, 38.611, 53.921, 55.138, 62.753,$ 68.807, 70.394, and 75.126) and PDF: 86-0148  $(2\theta = 27.462, 29.228, \text{ and } 39.228)$ , lattice structure was tetragonal, crystal sizes were 22.39 nm and 29.5 nm, respectively, as well as percent crystal and percent amorphous ratio being found to be 70.4:29.6 and 74.3:25.7, respectively. It is well known that crystal phase transformation from anatase to rutile phase occurs on calcination of TiO<sub>2</sub> at high temperatures [36, 49-51]. Both anatase and rutile phases are highly crystalline in nature, but anatase phase of titanium dioxide (TiO<sub>2</sub>) has its unique properties and is more effective in photocatalysis than rutile phase [52]. Catalyst M1B5 calcinated at 650°C (Fig. 2) possessed corresponding peaks of titanium oxide matched with JCPDS profile PDF: 86-0148 ( $2\theta = 27.445$ , 36.095, 41.256, 54.342, 56.646, and 69.032), PDF: 01-1167(38.204, 44.370, 64.179, and 77.549), crystalline phase of rutile/silver, and lattice structure of orthormbic/cubic. Crystal size of rutile was 23.09 nm as well as percent crystal and percent amorphous ratio found to be 59.40:40.5. Catalyst M1B6 calcinated at 750°C (Fig. 2) showed corresponding peaks of titianum oxide/silver, and crystal phase was identified as rutile/silver composite phase matched with JCPDS profile PDF: 86-0148  $(2\theta = 27.462, 36.127, 54.384, and 69.085)$ , PDF:  $87-0720 \ (2\theta = 38.201, 44.402, 64.602, and 77.600),$ lattice structure was composite of tetragonal/cubic, crystal size of rutile/silver composite catalyst was calculated as 26.32 nm as well as percent crystal and percent amorphous ratio found to be 70.3:29.7. When calcination temperature was increased up to 650°C and 750°C as a result of anatase peaks being suppressed (eventually degraded), rutile phase appeared on these calcination temperatures (650°C and 750°C) and showed a decrease in photocatalytic performance when used to treat synthetic textile effluent of Remazol red RGB (Fig. 5)

Accordingly, X-ray diffraction patterns of  $\text{TiO}_2$ and Ag-doped  $\text{TiO}_2$  used in immobilized applications (synthesized through another sol-gel route because



Degradation of synthetic effluent(Remazol Red RGB) under UV 400W with catalysts calcinated at different temperatures





Fig. 5. Photocatalytic degradation and decolorization of synthetic textile effluent with catalysts at 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures a) COD removal %. b) Color removal %.

Table 1. X-ray diffrectrom tric data of TiO, (mobilized) catalyst: 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C,
650°C and 750°C temperatures showing Corresponding Peaks, crystalline phase, structure/lattice, JCPDS, crystal size (nm), % crystal
and % amorphous.

Parameters		Catalyst calcinated at different temperatures								
Parameters	M1A1	M1A2	M1A3	M1A4	M1A5	M1A6				
Calcination temperature (°C)	0	350	450	550	650	750				
Correspond peak	NILL	Titanium oxide	Titanium oxide	Titanium oxide	Titanium oxide	Titanium oxide				
Cristalite Phase	NILL	Anatase,Syn	Anatase, syn	Anatase, syn	a) Rutile, syn b) Anatase, syn	a) Rutile, syn b) Anatase, syn				
Latice/Structure	Amorphous	Tetragonal	Tetragonal	Tetragonal	Tetragonal	Tetragonal				
JCPDS	-	PDF. 04-0477	PDF. 86-1157	PDF.86-1157	a) PDF.86-0148 b) PDF.86-1156	a) PDF. 86-0148 b) PDF. 86-1156				
Crystal size nm	0	9.34	14.83	18.01	22.39	29.5				
% Crystal	0	60.4	58.8	68.9	70.4	74.3				
% Amorphous	0	39.6	41.2	31.1	29.6	25.7				

a)

Table 2. X-ray diffrectromtric data of Ag-TiO<sub>2</sub> (mobilized) catalyst: 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures showing Corresponding Peaks, crystalline phase, structure/lattice, JCPDS, crystal size (nm), % crystal and % amorphous.

Parameters			Catalyst calcin	nated at different tempe	ed at different temperatures				
Farameters	M1B1 M1B2 M1B3 M1B4		M1B5	M1B6					
Calcination temperature (°C)	0	350	450 550		650	750			
Correspond peak	NILL	Titanium oxide	Titanium oxidea) Titanium oxideab) Silver		a). Titanium oxide b) Silver	a) Titanium oxide b) Silver			
Cristalite Phase	NILL	Anatase, syn	a). Anatase, syn b) Silver		a) Rutile,syn b) Silver	a) Rutile,syn b) Silver			
Latice/Structure	Amorphous	Tetragonal	Tetragonal	a) Tetragonal b) cubic	a) Tetragonal b)cubic	a) Tetragonal b) cubic			
JCPDS	-	PDF 78- 2486	PDF 86-1157	a) PDF 86-1157 b) PDF 87-0720	a) PDF 86-0148 b) PDF 01-1167	a) PDF 86-0148 b) PDF 87-0720			
Crystal size nm	0	13.82	14.6	23.19	23.09	26.32			
% Crystal	0	50.87	49.7	59.5	59.40	70.3			
% Amorphous	0	49.24	50.3	40.5	40.5	29.7			

of its performance and better gel adhesion on to the substrate) are shown in Figs 3 and 4.  $\text{TiO}_2$  and Ag-doped TiO<sub>2</sub> were coded as M2A1 and M2B1 (pulverized but not calcinated), M2A2 and M2B2 (calcinated at 350°C), M2A3 and M2B3 (calcinated at 450°C), M2A4 and M2B4 (calcinated at 550°C), M2A5 and M2B5 (calcinated at 650°C), and M2A6 and M2B6 (calcinated at 750°C).

Table 3 and 4 show the X-ray diffrectromtric data, with results revealing that no obvious diffraction peaks are observed in catalysts M2A1, M2A2, and M2B1 (Figs 3-4), and from this it is inferred that TiO, is amorphous.

X-ray diffractogram of M2B2 calcinated at 350°C (Fig. 2) indicates corresponding peaks of titanium oxide matched with JCPDS profile PDF: 78-2486 ( $2\theta = 25.307, 37.79, 48.043, 55.068, 62.689, 70.298$ , and

75.05), crystallite phase was anatase, lattice structure was tetragonal, crystal size was 8.39 nm, as well as percent crystal and percent amorphous ratio found to be 52.3:47.7.

Catalysts M2A3, M2A4, M2A5, and M2A6 calcinated at 450°C, 550°C, 650°C, and 750°C (Fig. 3) possessed corresponding peaks of titanium oxide matched with JCPDS PDF: 86-1157 ( $2\theta = 25.322$ , 37.863, 48.064, 53.975, 55.094, 62.758, 68.870, 70.330, and 75.141), PDF: 21-1272 ( $2\theta = 25.281$ , 37.801, 48.050, 53.891, 55.062, 62.690, 68.762, and 70.311), PDF: 86-1156 ( $2\theta = 25.335$ , 37.809, 48.104, 53.921, 55.138, 62.753, 68.807, and 70.394), and PDF: 86-5117 ( $2\theta = 25.322$ , 37.863, 48.064, 53.975, 55.094, 62.756, 68.870, 70.330, and 75.141), lattice structure was found as tetragonal, crystallite phase was anatase, crystal size was 11.31 nm,

Table 3. X-ray diffrectromtric data of TiO<sub>2</sub> (immobilized) catalyst: 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures showing Corresponding Peaks, crystalline phase, structure/lattice, JCPDS, crystal size (nm), % crystal and % amorphous.

D	Catalyst calcinated at different temperatures										
Parameters	M2A1	M2A2	M2A3	M2A4	M2A5	M2A6					
Calcination temperature (°C)	0	350	450	550	650	750					
Correspond peak	NILL	NILL	Titanium oxide	Titanium oxide	Titanium oxide	Titanium oxide					
Cristalite Phase	NILL	NILL	Anatase, syn	Anatase, syn	Anatase, syn	Anatase, syn					
Latice/Structure	Amorphous	Amorphous	Tetragonal	Tetragonal	Tetragonal	Tetragonal					
JCPDS	-	-	PDF 86-1157	PDF 21-1272	PDF 86-1156	PDF 86-1157					
Crystal size nm	0	0	11.31	13.26	20.53	23.27					
% Crystal	0	0	72	58.7	53.5	66.9					
% Amorphous	0	0	28	41.3	46.5	33.1					

Demonsterne			Catalyst calcinated at	different temperatures		
Parameters	M2B1 M2B2 M2B3 M2B4		M2B4	M2B5	M2B6	
Calcination temperature (°C)	0	350	450	450 550		750
Correspond peak	NILL	Titanium oxide	a) Titanium oxide / a) Titanium oxide / b) Silver b) Silver		Silver	Silver
Crystalite Phase	NILL	Anatase, syn	a) Anatase, syn b) Silver	a) Anatase, syn b) Silver	Silver	Silver
Latice/Structure	Amorphous	Tetragonal	a) Tetragonal b) Cubic	a) Tetragonal b) Cubic	Cubic	Cubic
JCPDS	-	PDF 78-2486	PDF 01-1167 PDF 01-0562	PDF 86-1157 PDF 87-0720	PDF 87-0720	PDF 87-0720
Crystal size nm	0	8.39	26.31	26.56	26.76	27.50
% Crystal	0	52.30	49.40	65.0	69.9	65.70
% Amorphous	0	47.70	50.60	35.0	30.10	34.30

Table 4. X-ray diffrectromtric data of Ag-TiO<sub>2</sub> (immobilized) catalyst: 0°C (without calcination), catalyst calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures showing Corresponding Peaks, crystalline phase, structure/lattice, JCPDS, crystal size (nm), % crystal and % amorphous.

13.26 nm, 20.53 nm and 23.27 nm, respectively, as well as percent crystal and percent amorphous ratio of 72:28, 58.7:41.3, 53.5:46.3, and 66.9:33.1, respectively.

M2B3 calcinated at 450°C (Fig. 4) showed corresponding peaks of titanium dioxide matched with JCPDS file PDF: 01-0562 ( $2\theta = 25.282$ , 37.934, 48.376, 53.888, 55.296, and 62.728) and PDF: 01-1167 ( $2\theta = 38.101$ , 44.370, and 64.179) and, TiO<sub>2</sub>/silver composite crystals were found, crystallite phase of titanium dioxide was anatase, lattice structure was found as tetragonal, crystal size was 26.31 nm, as well as percent crystal and percent amorphous ratio was 49.40:50.60.

Whereas, X-ray diffractrograms of M2B4 calcinated at 550°C (Fig. 4) possessed corresponding peaks of silver matched with JCPDS profile PDF: 86-1157 ( $2\theta = 25.322$ , 48.062, 55.094, 62.756, 68.870, and 76.08) and PDF: 87-0720 ( $2\theta = 38.201$ , 44.402, 64.602), titanium oxide/silver composite crystals were identified, crystallite phase was anatase, lattice structure was composite of tetragonal/ cubic, crystal size was 26.56 nm, as well as percent crystal and percent amorphous ratio found as 65.0:35.0.

M2B5 and M2B6 (Fig. 4) showed that silver was identified in corresponding peaks and matched with JCPDS profile PDF: 87-0720 ( $2\theta = 38.201$ , 44.402,

Table 5. Characteristics of synthetic textile effluent (Remazol Red RGB).

Parameter	Value
pH Initial dye conc.	3 10 ppm
COD (mg/L)	560
Absorbance (A 519 nm)	1.647

and 64.602) and PDF: 87-0720 ( $2\theta = 38.201$ , 44.402, and 64.602), lattice structure of silver identified as cubic, crystal size were 26.76 nm and 27.5 nm, respectively, as well as percent crystal and percent amorphous ratio found to be 69.9:30.10 and 65.7:34.30, respectively. At 550°C calcinations temperature silver and TiO<sub>2</sub> composite catalyst structure formed and gave optimum photcatalytic performance (Fig. 5), but as calcinations increased up to 650°C and 750°C anatase peaks disappeared due to phase change to rutile at high temperature, but X-ray diffractrogram showed only silver crystals because they grow in size with temperature and rutile crystals were suppressed.

# Photocatalytic Activity of TiO<sub>2</sub> and Ag- TiO<sub>2</sub>

The effect of calcination temperatures  $(350^{\circ}C, 450^{\circ}C, 550^{\circ}C, 650^{\circ}C, and 750^{\circ}C)$  on the performance of TiO<sub>2</sub> and Ag-TiO<sub>2</sub> catalysts was evaluated in terms of percentage removal of chemical oxygen demand (COD) and removal of colour of synthetic textile effluent (remazol red RGB) in a double-walled rectangular box reactor. Standard procedures given in "Standard methods were followed for the examination of water and wastewater" [53].

Photocatalytic activity of the catalysts was evaluated through degradation of a 1 litre sample of synthetic effluent (remazol red RGB) with initial dye concentration of 10 ppm, initial COD 560mg/l, pH of the effluent was adjusted at 3 as pH was optimized, and results are reported in our previous paper [46]. Photocataytic degradation was carried out under UV (400W) radiation.

Table 6 shows the results of maximum degradation and decolourization (COD removal percentage and color removal percentage), observed with the catalysts

				C	OD and O	Color rem	oval (%)	of synthe	tic textile	effluent			
Sr. No	Catalysts	00	PC	350	0°C	450	)°C	55(	)°C	650	)°C	75	0°C
		COD	Color	COD	Color	COD	Color	COD	Color	COD	Color	COD	Color
1	TiO <sub>2</sub> (mobilized)	12.32	5.89	28.57	18.03	49.29	33.22	84.11	44.46	42.86	24.10	40.0	19.85
2	Ag-TiO <sub>2</sub> (mobilized)	17.5	10.75	51.43	22.89	59.29	38.07	86.07	99.57	68.21	32.60	71.43	23.49
3	TiO <sub>2</sub> (immobilized)	6.6	4.07	14.29	14.39	38.21	25.32	79.43	78.25	46.61	44.14	38.93	16.21
4	Ag-TiO <sub>2</sub> (immobilized)	18.39	8.32	48.57	19.25	55	41.11	91.96	90.15	62.86	26.53	57.50	14.99

Table 6. COD removal (%) and Colour removal (%) of the synthetic effluent (catalyst dose 0.5 g and 60 min irradiation time) degraded with catalysts 0°C (without calcinations) and calcinated at 350°C, 450°C, 550°C, 650°C and 750°C temperatures.

Table 7. Statistical Descriptive analysis: value of mean (M) and standard deviation (SD) of factors "calcinations temperature" as catalyst was calcinated at different temperatures and labelled in SPSS software as catalysts  $0^{\circ}C = 1$  (without calcinations) and calcinated at  $350^{\circ}C = 2$ ,  $450^{\circ}C = 3$ ,  $550^{\circ}C = 4$ ,  $650^{\circ}C$  and  $750^{\circ}C = 5$  temperatures.

Parameters	Mean (M) $n = 24$	Standard Deviation (SD) n = 24
Calcination temperature	3.5	1.74

calcinated at 550°C. It is observed that with increased calcination of the catalysts up to a certain temperature increases its photcatalytic activity.

TiO<sub>2</sub> (mobilized), Ag-TiO<sub>2</sub> (mobilized), TiO<sub>2</sub> (immobilzed), and Ag-TiO<sub>2</sub> (immobilzed) calcinated at 550°C showed maximum performance at optimum treatment conditions (UV-400W radiataion, volume of the effluent 1 litre, catalyst load 0.5 gram, catalyst mesh (with four layers coating of TiO<sub>2</sub> and Ag-TiO<sub>2</sub>), pH of effluent 3, initial COD 560 mg/l, and temperature was maintained ranging between 29-32°C during treatment).

Results shown in Table 6 and Fig. 5(a-b) illustrate that the obtained percentage removal of COD (color) values were 84.11% (44.46%), 86.07% (99.57%), and 79.43% (78.25%), 91.96% (90.15%) for TiO<sub>2</sub> (mobilized), Ag-TiO<sub>2</sub>(mobilized), TiO<sub>2</sub> (immobilzed), and Ag-TiO<sub>2</sub> (immobilzed), respectively. Results also revealed that Ag-TiO<sub>2</sub> doped catalysts showed much better results among the rest of the catalysts as shown in Fig. 5(a-b).

Fig. 5 represents COD and color removal percentage of synthetic textile effluent photocatalytic system. Results of photocatalytic degradation of the synthetic textile effluent (remazol red RGB) with initial dye concentration of 10 ppm, COD concentration of 560 mg/l, at pH 3 revealed that catalysts calcinated at different temperatures performed differently during the degradation and decolorization process (Table 6, Fig. 5). At calcination temperature of 350°C all catalysts showed low catalytic degradation as well as low decolourzation, which is evidence of low catalytic activity, except the catalyst calcinates at 550°C. It is also revealed that along with increasing calcination temperature, catalytic the activity increased until 550°C, at which point the highest photocatalytic activity is observed. Furthermore, catalysts calcinated at 650°C and 750°C didn't show

Table 8. One-way ANOVA results of COD removal and color removal percentage with respect to the factor "Calcination temperature".

Variables							
variables		Sum of Squares	Df	Mean Square	F	Sig. (P<0.05)	Decision
COD removal %	Between Groups	11179.575	5	2235.915	15.981	.000	Significant mean difference
	Within Groups	2518.420	18	139.912			
	Total	13697.996	23				
Color removal %	Between Groups	12398.186	5	2479.637	20.046	.000	Significant mean difference
	Within Groups	2226.575	18	123.699			
	Total	14624.761	23				

	-	
Sr. No.	Significance Mean difference between the Groups	<i>p&lt;0.05</i>
1	0°C VS 450°C	0.004
2	0°C VS 550°C	0.000
3	0°C VS 650°C	0.001
4	0°C VS 750°C	0.003
5	550°C VS 0°C	0.000
6	550°C VS 350°C	0.000
7	550°C VS 450°C	0.006
8	550°C VS 650°C	0.021
9	550°C VS 750°C	0.009

Table 9. The results of the Tukey post hoc tests (multiple comparison) dependent variable: COD % removal (Tukey HSD).

Table 10. The results of the Tukey post hoc tests (multiple comparison) dependent variable: Color removal percentage (Tukey HSD).

Sr. No.	Significance Mean difference between the Groups	<i>p</i> <0.05
1	0°C VS 450°C	0.029
2	0°C VS 550°C	0.000
3	550°C VS 0°C	0.000
3	550°C VS 350°C	0.000
4	550°C VS 450°C	0.000
5	550°C VS 650°C	0.000
6	550°C VS 750°C	0.000

much increase in percentage removal in degradation and decolourization. Results from Table 1-4 and Figs 1-4 also reveled that at 550°C calcinations temperature anatase crystalline phase is dominating and crystaline size increased slowly as a result of performance of the catalysts proven to be in favor of photocatalytic degradation and decolourization of the synthetic effluent shown in Table 6 and Fig. 5(a-b).

Results of XRD patterns give evidence that anatase crystal phase of  $\text{TiO}_2$  was obtained at 550°C calcination temperature. We concluded that the higher photocatalytic activity of  $\text{TiO}_2$  is due to the parameter of calcination temperature to obtain the required crystalline phase. Photocatalytic activity was obtained better in the anatase phase of  $\text{TiO}_2$  for the degradation of all substances as compared with the rutile phase. Photocatalytic degradation of dyes and organic contaminants in water using nanocrystalline anatase and rutile  $\text{TiO}_2$ [54].

The activity of  $\text{TiO}_2$  and  $\text{Ag-TiO}_2$  highly depends on its crystal phase. The particle size of the catalyst also plays a very important role in its photocatalytic activity. A decrease in particle size results in large surface area, which is favorable for high photocatalytic activity. Based on XRD data and performance in photocatalytic activity of catalysts it is revealed that a calcination temperature of 550°C with small crystal size is most effective.

# Statistical Analysis

The descriptive analysis of the results was carried out through SPSS (V15) in terms of mean, standard deviation, analysis of variance (ANOVA). Statistical correlations between groups were calculated using oneway ANOVA. According to the descriptive analysis, the mean and standard deviation values for the parameter "calcination temperature" are M = 3.5 and SD = 1.74, respectively. The values of calcination temperature mean = 3.5 indicates that results of the treatment are in favour of the catalyst calcinated at 550°C, as well as the SD = 1.74 indicating that the overall treatment results obtained by using catalyst calcinated at 550°C are not scattered (Table 7).

Analysis of variance (ANOVA) with F values of 95% significance level ( $\alpha = 0.05$ ) is used to statistically evaluate the experimental data of chemical oxygen demand (COD) and color removal percentage. Analysis revealed that catalyst calcinaed at 550°C showed optimum results for degradation and decolourization of synthetic effluent (remazol red RGB). Results were compared through one-way ANOVA tests (Statistics 15; SPSS Inc. Package) (Table 7). According to the results, there was a significant effect of "calcination temperature" (p < 0.05) as p-value is 0.000 (F = 15.981) on degradation and decolourization of the effluent, which is less than the significance level of 0.05 (Table 8). These values indicate that there is a significance mean difference between the COD removal percentage values when considering the parameter of the calcination temperatures (0°C, 350°C, 450°C, 550°C, 650°C, and 750°C (Table 8). Thus, a post hoc test reveals that the significance difference found at the level p<0.05 in the results of the COD removal and color removal percentage obtained when synthetic effluent was treated with the catalysts calcinated at 0°C and 550°C (Table 9 and 10).

Significant mean values are mentioned in Table 9, which are less than the level of significance (p<0.05), which shows that there is a major difference present in the results of COD removal percentage between 0°C (p<0.05) VS 450°C, 550°C, 650°C, and 750°C. As well as between 550°C (p<0.05) VS 0°C, 350°C, 450°C, 550°C, 650°C, and 750°C. We also found that there is a large significant mean difference found between 0°C (p<0.05) VS 550°C (p<0.05) for the results of COD removal percentage. This indicates that optimum COD removal percentage was achieved with catalyst calcinated at 550°C.

Results of color removal percentage are shown in Table 10. We found that values of color removal percentage obtained from the treatment carried out using catalysts calcinated at 0°C (p<0.05) have significant mean difference with the results obtained from catalysts calcinated at 450°C and 550°C. There is also another difference found between values of color removal percentage in the catalyst calcinated at 550°C (p<0.05) VS 0°C, 350°C, 450°C, 550°C, 650°C, and 750°C. From Table 10 we infer that a major difference in the results of color removal percentage is achieved between 0°C VS 550°C, which indicates that optimum colour removal percentage was achieved by using catalyst calcinated at 550°C.

#### Conclusions

The higher photocatalytic activity of TiO<sub>2</sub> is due to the parameter of calcination temperature to obtain the required crystalline phase. Photocatalytic activity was obtained better in anatase phase of TiO<sub>2</sub> for the degradation of all substances as compared with rutile phase. Results have given evidence that anatase crystal phase of TiO<sub>2</sub> was obtained at 550°C calcination temperature. The activity of TiO, and Ag-TiO, highly depends on its crystal phase. The particle size of the catalyst also plays a very important role in its photocatalytic activity as small particle size results in large surface area, which is favorable for high photocatalytic activity. Based on XRD data and performance in photocatalytic activity of catalysts, it is revealed that calcination temperatures of 550°C with small crystal size are most effective. TiO, and Agdoped TiO<sub>2</sub> proved to be very effective catalysts in photocatlytic degradation of synthetic textile effluent. The photocatalytic activity of catalysts found in results with respect to their calcination temperatures can be stated in the following order:  $550^{\circ}C > 450^{\circ}C > 650^{\circ}C >$  $750^{\circ}C > 350^{\circ}C > 0^{\circ}C$ . Moreover, maximum photocatalytic activity was achieved by catalysts calcinated at 550°C as 91.96% degradation (COD removal percentage) with Ag-doped TiO, immobilized catalyst and 99.57% decolorization (colour removal percentage) was achieved with Ag-doped TiO<sub>2</sub> mobilized catalyst on 60 min treatment of synthetic textile effluent (Remazol red RGB: 10 ppm concentration, pH3). This is because of the presence of Ag doping and anatase crystalline phase of TiO<sub>2</sub>, which favored degradation and decolourization. The order of degradation and decolourization at 550°C found out as Ag-TiO<sub>2</sub> (immobilized) > Ag-TiO<sub>2</sub> (mobilized) >  $TiO_2$  (mobilized) >  $TiO_2$  (immobilized) and Ag-TiO<sub>2</sub> (mobilized) >Ag-TiO<sub>2</sub>(immobilised)> TiO<sub>2</sub> (immobilized) > TiO<sub>2</sub> (mobilized), respectively.

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#### **Conflict of Interest**

The authors declare no conflict of interest.

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