Original Research The Influence of Chemical Modification on the Co²⁺ Ion Sorption Process by Anaerobic Sludge

Vladimír Frišták*, Michaela Valovčiaková, Martin Pipíška, Juraj Lesný

Department of Ecochemistry and Radioecology, Faculty of Natural Sciences, University of SS. Cyril and Methodius in Trnava, Nám. J. Herdu 2, SK-917 01, Trnava, Slovak Republic

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Abstract

Modification by chemical agents affected the sorption capacities of sludge from municipal wastewater treatment plants (WWTPs). We tried to characterize changes in sorption capacity of dried anaerobic sludge (DANS) after chemical modification by formaldehyde, methanol, and hydrochloric acid. Modified sludges were characterized by FT-IR spectroscopy, cation exchange capacity, and electrothermal atomic absorption spectrometry (ETAAS) analysis. Maximum sorption capacities Q_{max} at pH 6.0 for Co²⁺ ions calculated from Langmuir isotherm model were 175±5 µmol/g for unmodified DANS, 170±2 µmol/g for CH₂O-modified DANS, 12±0.2 µmol/g for CH₃OH-modified DANS, and 15±0.3 µmol/g for HCl-modified DANS. Our paper established the crucial role of carboxyl functional groups against amino and hydroxyl groups in sorption process of cobalt ions.

Keywords: anaerobic sludge, sorption, Co²⁺, chemical modification FT-IR

Introduction

Production of unsettleable sludges in wastewater treatment plants (WWTPs) as a result of industrial intensification presents a serious problem for environmental protection. Sludge utilization is limited by content of heavy metals. Generally, these wastes can be utilized as soil fertilizers and conditioners. The Ministry of the Environment of the Slovak Republic (2010) showed that the total annual production of sewage sludge in SR is around 55,000 t of dry matter per year. The major part of sludge production is composted. Most authors [1-4] described the utilization of sewage sludges from WWTPs as an efficient sorbent of heavy metals and emerging organic compounds from liquid wastes and industrial waste waters. Anaerobic sludges contain variable amounts of bacteria, protozoa, and extracellular polymeric substances [5]. Extracellular polymers are a matrix of proteins, carbohydrates, humic, and nucleic acids [6]. These components play an important role in the formation of anaerobic sludge structures and are rich in active centers of xenobiotic binding. Conventional methods for toxic metals removal from aqueous solutions as precipitation, ionexchange, electrochemical pretreatment, or ultrafiltration are not all fully effective and have a lot of limitations. The main disadvantages of classical methods are low efficiency of the removal process when toxic metal concentrations are in the range of 1-100 mg/L [7] and production of toxic sludges. Sorption as a potential alternative to the classical toxic metal removal has several advantages [8].

Our the paper [9] shows different modes of the sorption process such as nonactive metal uptake by biomass. Utilization of microbial sorbents and extracellular polymer

^{*}e-mail: vladimir.fristak@ucm.sk

substances has a crucial role in sorption processes and sorbent preparation. Authors [10, 11] refer to the ability of living organisms to uptake cobalt ions from liquid wastes. Both living and dead microbial biomass shows high sorption capacity. The toxic effect of high concentration of heavy metals to living cells is one of the limitations of biosorption and bioaccumulation utilization in remediation studies. To overcome the disadvantages, dead biomass is preferred in removal of toxic compounds and metals [12]. Many authors [13-15] showed the importance of superficial functional groups of organic matter in sorption processes of heavy metals. The presence of carboxyl (-COOH), hydroxyl (-OH), aldehyde (-COH), sulfhydryl (-SH), and amino (-NH₂) is decisive for binding bivalent ions. Acidic functional groups of sorbents are involved in metal binding and there exists a positive correlation between their total concentration and the process of biosorption [16]. Sorption capacities of sorbents can be changed by a wide range of treatments methods. Modification of biomass using physical methods such as heating, autoclaving, freezing, drying, boiling, and chemical treatment such as effects of acids, alkalis, and organic chemicals showed reduction in heavy metal sorption [17]. Chemical pretreatments of sludge can predict sorption behavior of sorbent under reaction conditions of chemical agents present in waste waters. In addition, dried anaerobic sludge could provide economic sorbent, however, solubilization and leaching of organic compounds can cause the pollution in the second step.

Thus, it is preferable to treat sludge by chemical modification agents that influence the concentration of solubilized sludge fractions as well as capacity of sorption material. The main aim of this paper was to point out the influence of chemical modification on Co^{2+} ions sorption process by dried anaerobically digested sludge. A lot of scientific discussions show the ability of specific chemical agents to block typical functional groups of sorbents. We tried to characterize sorption mechanisms of Co^{2+} ions as a model of bivalent heavy metal ions from a single metal system by dried anaerobic sludge before and after chemical modification by formaldehyde, methanol, and hydrochloric acid.

Materials and Methods

Biosorbent Preparation and Modification

Biomass of anaerobically digested sludge was obtained from municipal WWTP (Zeleneč, Slovak Republic). After washing twice in deionized water, sludge was oven dried at 90°C for 48 h, ground, and sieved. Powdered dried anaerobic sludge (DANS 1) of particle size <450 μ m was used for Co²⁺ ion sorption studies. For chemical modification of sludge biomass, solutions of CH₂O (DANS 2), 96% CH3OH (DANS 3), 0.1 mol/L HCl (DANS 4) were used. Preparation of modified sorbents was carried out by suspending dried anaerobically digested sludge (fraction <450 μ m) in chemical agents (ratio w/v sludge: agent, 1:40) and agitation for 6 h at 22°C, 150 rpm. After reaction time, liquid phase was removed and washed sediment of modified sludge sorbents was dried at 90°C for 48 h. Powdered modified anaerobic sludges of particle size <450 μ m were used for Co²⁺ ion sorption studies. Chemical reagents used to modify anaerobic sludge including formaldehyde, anhydrous methanol and hydrochloric acid were all purchased from Merck (SK). All agents were analytical grade and without further purification.

Biosorbent Characterization

Soluble fractions in 0.9% NaCl at 22°C of the sludges were characterized by determinations of soluble protein [18], carbohydrate [19], -SH contents [20], and soluble inorganic salt contents determined by ion chromatography (IC) using Dionex ICS-5000 RFIC, Reagent-FreeTM Ion Chromatography (Dionex – Thermo Fisher Scientific, USA). Solid fractions of sorbents prepared from DANS were characterized for cobalt initial content by ETAAS analysis using a Shimadzu AA-6300 (USA).

Cation exchange capacities (CEC) were estimated according to the Slovak Institute of Metrology modified by Frišták et al. [1]. Sludge sorbents (DANS 1-4) were suspended (83.3 g/L) in 0.1 mol/L BaCl₂ and mixed on a laboratory shaker for 1 h at 22°C at 150 rpm. Phases were separated after centrifuging (5 min at 5,000 rpm). This procedure was repeated twice. The next step of CEC determination consisted of resuspending sludge sediments in 3 ml of 0.025 mol/L BaCl₂ and of agitation for 19 h at 22°C. After phase separation, 3 ml of 0.02 mol/L MgSO₄ was added to sediments. After agitation (19 h at 22°C), centrifuging and phase separation, CEC by standardized 0.02 mol/L Na₂EDTA was determined. The CEC values were determined by chelatometric determination of Mg²⁺ ions in liquid phase and calculated according to:

$$CEC = \frac{\left(M_0 V_0 - M V_{\nu}\right)\varepsilon}{10^{-3}} \tag{1}$$

...where CEC is cation exchange capacity (meq 100 g⁻¹), M_0 is molar concentration of magnesium added to the sample (mol·L⁻¹), V_0 is volume of solution of magnesium added to the sample (L), M is molar concentration of the magnesium in the leachate (mol·L⁻¹), V_v is volume of obtained extract (L), and ε is the conversion factor that has for the bivalent ions and amount 0.25 g of sorbent value 800 meq (100 g·mol⁻¹).

Sorption Experiments

Batch sorption experiments from a single metal system were carried out by suspending DANS 1-4 biomass (2.5 g /L, d.w.) in water solutions of $CoCl_2$ in concentration 1000 µmol/L spiked with radionuclide ⁶⁰Co (70 kBq/L) and adjusted to desired pH 6. Flasks were agitated on reciprocal shaker (120 rpm) at 22°C for 4 h and samples were taken for equilibrium study. Biomass was filtered out, washed twice in deionised water, and radioactivity of sludges was measured. The batch experimental set-up to determine the sorption capacity of sludges was described in detail previ-

Isotherm model	Equation	Parameters			
Langmuir model		Q_{eq} – amount of sorbed sorbate at equilibrium			
	$Q_{eq} = \frac{bQ_{\max}C_{eq}}{1 + bC_{eq}}$	B – coefficient related to the affinity between metal ion and the sorbent			
		Q_{max} – maximum metal uptake capacity			
		C_{eq} – equilibrium concentration in metal solution			
Freundlich model	$Q_{eq} = K C_{eq}^{(1/n)}$	Q_{eq} – amount of sorbed sorbate at equilibrium			
		C_{eq} – equilibrium concentration in metal solution			
		K, n – Freundlich empirical constants indicating sorption capacity and intensity of sorption			

Table 1. Equations of adsorption isotherms.

Table 2. Physico-chemical characteristics of studied sorbents DANS 1-4.

Sorbent	Solid fraction		Soluble fraction ^{a)}					
	CEC ^{b)} [meq/100g]	Co content ^{c)} [µg/g]	Proteins ^{d)} [mg/g]	Carbohydrates ^{e)} [mg/g]	Thiols ^{f)} [µmol/g]	Anions ^{g)} [µg/L]		
DANS 1	25	<1	9.6	5.1	6.1	<lod< td=""></lod<>		
DANS 2	24	<1	<0.5	4.5	<1	<lod< td=""></lod<>		
DANS 3	0.5	<1	<0.5	4.2	<1	<lod< td=""></lod<>		
DANS 4	2	<1	<0.5	5.0	<1	<lod< td=""></lod<>		

^{a)} extracted by 0.9% NaCl at 22°C; ^{b)} cation exchange capacity determined by $BaCl_2$; ^{c)} initial concentration of cobalt (ETAAS); ^{d)} determination of soluble proteins; ^{e)} determination of carbohydrates by anthrone reagent; ^{f)} determination of thiols by 5,5-dithiobis-(2-nitrobenzoic acid); ^{g)} determination of soluble inorganic salts by IC (values of LOD for anions used (μ/L): fluorides 6, chlorides 7, nitrites 20, bromides 29, sulphates 25, nitrates 24, phosphates 7)

ously [1]. All experiments were performed in triplicate. The metal uptake was calculated as:

$$Q_{eq} = (C_0 - C_{eq})\frac{V}{M}$$
(2)

...where Q is the uptake (µmol/g), C_0 and C_{eq} are the liquidphase concentrations of metal at initial and equilibrium (µmol/L), V is the volume (L), and m is the amount of dried biosorbent (given in grams).

Radiometric Analysis and FT-IR Analysis

The gamma spectrometric assembly using a well-type scintillation detector 54BP54/2-X, NaI(Tl) (Scionix, the Netherlands) and Scintivsion 32 data processing software (ORTEC, USA) were used for ⁶⁰Co determination in DANS 1-4 at the energy of γ - photons: ⁶⁰Co – 1,173.24 keV. Standardized ⁶⁰CoCl₂ solution (5.181 MBq/ml; 20 mg CoCl₂/L in 3 g·dm⁻³ HCl) was obtained from the Czech Institute of Metrology. The spectrometric analysis of sorbents in infrared region (FT-IR) was carried out to identify the chemical functional groups present on non-treated and pretreated sorbents and to explain the sorption mechanism. FT-IR spectra of unloaded and Co-loaded sorbents were performed by KBr technique using Nicolet NEXUS 470 spectrometer.

Data Analysis

Data analysis of adsorption equilibrium was done using Langmuir and Freundlich adsorption isotherm equations (Table 1). To calculate maximum sorption capacity of sorbents and the corresponding parameters of adsorption isotherms, non-linear regression analysis was performed by ORIGIN 8.0 Professional (OriginLab Corporation, Northampton, USA).

Results and Discussion

Physico-Chemical Characterization of Sorbents

Characterization of unmodified and modified sorbents DANS 1, DANS 2, DANS 3, and DANS 4 used in paper are present in Table 2. The initial concentrations of cobalt in studied sorbents were lower than the detection limit (LOD) of ETAAS detector, which was 1 μ g of Co per g of d.w. It suggests the ability of free binding sites for Co²⁺ ions. The cation exchange capacity of unmodified DANS 1 was 25 meq per 100 g of d.w., which is higher than CEC of dried activated sludge from industrial WWTP [1]. According to Eq. 1 values of CEC decreased in the order DANS 1 > DANS 2 > DANS 4 > DANS 3. The effects of chemical modification by CH₂O (DANS 2) caused minimal changes

Sorbent	Model	Q _{max} [µmol/g]	b [L/µmol]	<i>K</i> [L/g]	1/ <i>n</i>	\mathbb{R}^2
DANS 1	Lagmuir	175±5	0.003±0.001		—	0.966
DANS I	Freundlich	_	_	21.91±4.01	0.25±0.13	0.756
DANS 2	Lagmuir	170±2	0.004±0.001	_	—	0.987
DANS 2	Freundlich	_	_	18.45±3.54	0.24±0.13	0.747
DANS 3	Lagmuir	12±0.2	0.0003±0.0001	_	_	0.989
	Freundlich	—	_	3.14±0.17	0.14±0.02	0.886
DANS 4	Lagmuir	15±0.3	0.0002±0.0001	_	_	0.998
	Freundlich	—	—	3.39±0.12	0.16±0.04	0.921

Table 3. Langmuir and Freundlich equilibrium parameters (\pm standard deviation of the mean) for Co²⁺ ions sorption by studied sorbents obtained by non-linear regression analysis.

in exchange capacity of sludge. Methylation of DANS amino and hydroxyl functional groups by formaldehyde as a crosslinking agent had a non-significant effect on CEC value. On the other hand, esterification of carboxylic functional groups of DANS by methanol caused a decrease of CEC value of about 98%. Cation-exchange capacity equally decreased after hydrochloric acid modification by more than 90%. Inorganic acids can cause irreversible damage of sorbent surface that in turn decreased the concentration of exchangeable ions. As shown in Table 2, concentrations of water-soluble proteins and carbohydrates sorbents used in the experiments decreased after chemical modification. Contents of soluble proteins and thiols of DANS 2, DANS 3, and DANS 4 were lower than LOD of used methods. In addition, determination of soluble inorganic salts by IC at ambient temperature confirmed the absence of fluorides, chlorides, nitrites, bromides, sulphates, nitrates, and phosphates in salt solutions of sorbents.

Sorption Process and Role of Functional Groups

Sorption capacity of the sorbent is one of the most important factors for its practical utilization. Physical, chemical, or biological pretreatments can increase or decrease capacity for uptake of toxic metals by sewage sludge-based sorbents [21]. A number of modification reagents such as hydroxides and carbonates (NaOH, CaOH₂, Na₂CO₃), mineral and organic acids (HCl, HNO₃, H₂SO₄, EDTA, C₆H₈O₇), organic compounds (ethylene, formaldehyde, methanol, acetone), oxidant (H₂O₂), and dyes (Orange 13) can be used for chemical modifications [22]. Modification of sorbent surfaces by chemical agents is a possibility of sorption capacity changes [23]. Increased surface area of sludge is related to increased concentration of weak acidic functional groups of sorbents. In pursuance of our previous papers [1, 4, 24], we defined that the sorption of cobalt ions by DANS is a rapid process in which the equilibrium is reached within 2 h (Fig. 1). Experimentally estimated sorption capacities of DANS 1-4 for cobalt ions were calculated according to Eq. 2. and fitted to nonlinear forms of the Langmuir and Freundlich adsorption isotherms. Coefficients of determination indicated that the Lagmuir model fits obtained data better in comparison with the Freundlich model (Table 3).

To determine maximum sorption capacities (Q_{max}) of studied sorbents the theoretical Lagmuir isotherm was used. Q_{max} value of unmodified DANS for Co²⁺ ions was 175 µmol/g. We found the effects of chemical modifications to Q_{max} values of studied sorbents for Co²⁺ ions. Bhatti et al. [25] showed that formaldehyde can enhance uptake capacity of sludge biomass by increasing the surface area and porosity of original samples, but our sorption data for DANS 2 did not confirm this fact.

We found modification of sludge biomass by formaldehyde and thus the blocking of hydroxyl and amino functional groups caused a non-significant decrease in cobalt



Fig. 1. Effect of contact time on sorption of Co^{2*} ions by DANS 1 (**D**), DANS 2 (**O**), DANS 3 (**O**), DANS 4 (**D**) in a single metal system. Experimental conditions: $c_0 = 1000 \ \mu \text{mol/L} \ \text{CoCl}_2$, amount of sorbent 2.5 g/L, ⁶⁰CoCl₂ 70 kBq/L, pH 6, reaction time of 10-1,440 min, at 22°C. All experiments were performed in triplicate. Error bars represent standard deviation of a mean (±SD).

Sorbent	Q_{max} [µmol·g ⁻¹]	Reference	
Activated sludge from distillery WWTP	256±9	[1]	
Anaerobicically digested sludge from distillery WWTP	209±5	[2]	
Anaerobically digested sludge from municipal WWTP	175±5	This paper	
Methylated anaerobically digested sludge from municipal WWTP	170±2	This paper	
Esterified anaerobically digested sludge from municipal WWTP	12±0.2	This paper	
0.1 HCl treated anaerobically digested sludge from municipal WWTP	15±0.3	This paper	

Table 4. Comparison of maximum sorption capacity (Q_{max}) of select sludge sorbents for Co²⁺ ions.

sorption. Comparison of Q_{max} values of DANS 1 and DANS 2 (Table 3) showed the absence of hydroxyl and amino functional groups in sorption process of Co²⁺ ions by DANS. Pérez-Marín et al. confirmed the negligible effect of hydroxyl groups on Cd, Cr, and Zn sorption onto orange waste [26]. Hydrochloric acid (DANS 4) removed not only impurities from sludge surface but also released extracellular polymers after rupturing the cell-membrane and causing significant damage to sorbent [11]. Esterification of carboxyl functional groups by methanol (DANS 3) caused a significant decrease of Q_{max} , about more than 94%. Sorption capacities of dried activated sludge for Cd²⁺ and Zn²⁺ ions

before and after methanol treatment are not similar [4]. Authors showed reduction of both Zn^{2+} and Cd^{2+} ions adsorbing about 43% and 34% by esterified carboxyl groups of sludge surface. Kiliç et al. also found out effect of carboxyl group modification by esterification. Authors showed the deacreasing of sludge sorption capacity after chemical modification and confirmed the major role of carboxylic groups in Pb²⁺ ions sorption [27]. Q_{max} values of modified and unmodified anaerobically digested sludges are comparable to other sludge sorbents (Table 4). Hullebusch et al. found maximum sorption capacity of anaerobic sludge granules for Co²⁺ ions as 209 µmol/g.



Fig. 2. FT-IR spectra of DANS 1(A), DANS 2 (B), DANS 3 (C), DANS 4 (D) before (solid line) and after (dashed line) sorption of Co^{2+} ions ($c_0 = 4,000 \mu mol/L CoCl_2$, DANS 2.5 g/L d.m., reaction time 4 h).

	v/cm ⁻¹							
Type of vibration/	DANS 1		DANS 2		DANS 3		DANS 4	
functional group	Before sorption*	After sorption*	Before sorption*	After sorption*	Before sorption*	After sorption*	Before sorption*	After sorption*
Valence vibration –OH, –NH	3,423	3,429	3,421	3,420	3,399	3,399	3,422	3,422
Asymmetric vibration aliphatic CH ₂ , CH ₃	2,924	2,925	2,927	2,925	2,924	2,925	2,921	2,920
Symmetric vibration aliphatic CH ₂ , CH ₃	2,852	2,854	2,854	2,854	2,855	2,856	2,845	2,846
Valence vibration C=O (carboxylates)	1,745	1,747	1,748	1,750	1,748	1,748	1,740	1,742
Valence vibration C=O, C-N (amide I)	1,657	1,658	1,658	1,658	1,658	1,658	1,654	1,654
Valence vibration C=O, C-N	1,536	1,538	1,539	1,538	1,539	1,539	1,531	1,531
(amide II)	1,518	1,517	1,517	1,517	1,518	1,518	1,516	1,516
Valence vibration C=O, -OH (phenols)	1,452	1,448	1,448	1,449	1,450	1,450	1,450	1,450
Valence vibration C=O, -OH	1,230	1,220	1,219	1,223	1,221	1,220	1,229	1,226
Valence vibration –OH, C–O–C (esters)	1,078	1,090	1,090	1,090	1,092	1,092	1,074	1,074

Table 5. Wavenumber values ν/cm^{-1} of unmodified (DANS 1) and modified sorbent (DANS 2-4) with expected functional groups; FT-IR spectra in Figs. 2 a, b, c, and d.

*before and after sorption of Co2+ ions (4,000 µmol/L CoCl₂, 4 h, pH 6±0.05, 22°C) by DANS 1-4 (2.5 g/L).

To confirm obtained experimental data, FT-IR analysis of studied sorbents before and after Co2+ ion sorption in the range of 4000-400 cm⁻¹ was used. DANS spectra are sketched out in Fig. 2 (a-d). The compounds deciphered could be identified based on the reports in previous study and are shown in Table 5. The profile in Fig. 2a portrays the FT-IR spectrum of unmodified sludge (DANS 1). The strong band at 3,423 cm⁻¹ reflected N-H and O-H stretching vibrations of hydroxyl and amine groups on the surface of the anaerobic sludge, while the band at 2,924 cm⁻¹ and the band at 2,852 cm⁻¹ represented asymmetric and symmetric vibrations of CH₂ and CH₃. The band at 1,745 cm⁻¹ could be assigned to the valence vibration of C=O of carboxylates. A distinct band at 1,657 cm⁻¹ is the result of the valence vibration of C=O and C-N (amide I) peptidic bonds of proteins. Wavenumber of 1,536 cm⁻¹ band could be due to a combination of the valence vibration of C=O and deformation vibration C-N (amide II). The band at 1,230 cm⁻¹ could be attributed to the O-H stretching of phenols. Band at 1,078 cm⁻¹ could be attributed to the stretching vibration of -OH of esters.

After sorption of Co²⁺ ions were distinct shifts attributed to the vibration of carboxyl, amino, and hydroxyl groups (Table 5). Treatment of sludge with formaldehyde (DANS 2) changes the methylation of amine group (Fig. 2b). The band at 3,421 cm⁻¹, 1,658 cm⁻¹ and 1,539 cm⁻¹ got wider and the apex was lower compared to DANS 1. This modification demonstrates that O–H and N–H groups were reduced. In addition, FT-IR spectrum of DANS 2 after sorption process of Co²⁺ ions confirmed insignificant shifts of amide I and amide II bands. There was a substantial decrease in adsorption intensity of carboxyl groups at 1,748 cm⁻¹ and 1,219 cm⁻¹. Comparison of sorption experiments and FT-IR analysis of DANS confirmed only minimal effect of methylation of amino and hydroxyl groups to sorption process of Co²⁺ ions. On the other hand, modification of sludge with methanol (DANS 3) changes the esterification of carboxyl groups (Fig. 2c).

Observed bands at 1,748 cm⁻¹ and 1,450 cm⁻¹ substantially shifted and the two bands became wider and lower, which may be attributed to the esterification of carboxyl groups in the anaerobic sludge. The FT-IR spectrum of DANS 3 after sorption Co2+ ions and experimentally obtained values of Q_{max} after esterification of carboxyl groups indicate that functional groups of carboxylates play a crucial role in the sorption process of cobalt ions. The effect of esterification of carboxyl groups on the biosorption process of heavy metals is very important [28]. Modification of DANS by hydrochloric acid can be used as a tool to lower the inorganic content of a carbonaceous material through partial dissolution of the inorganic fraction [29]. The analysis of FT-IR spectrum of DANS 4 (Fig. 2d) revealed that hydrochloric acid as a chemical agent caused the crucial changes in width and intensity of bands of amide I and II. After sorption of Co2+ ions, minimal shifts of carboxyl groups at v 1,740 and 1,229 cm⁻¹ were detected (Table 4). Less significant shifts of carboxyl functional groups after metal sorption can occur due to the presence and interaction of Ca2+ and Mg2+ ions in the ion exchange process of Co2+ ions [24].

Xu and Liu showed the influence of electrostatic interactions between the hydroxyl and carboxyl functional groups on sorption of Cd^{2+} , Cu^{2+} , and Ni^{2+} by aerobic granules [30]. Sorption experiments confirmed a decrease of sorption capacity of DANS 4. The treatment of sludge by hydrochloric acid can yield dramatic improvements in sludge surface areas [29] but can also significantly damage the sorption surface and released the oxygen complexes and polymer substances (proteins and phosphates) [24, 25]. Sludge electronegativity decreases due to increased concentration of H^+ ions present in the structures of DANS. Changes of biomass electronegativity caused the decrease of sorption capacity of sorbents [31]. Benguella and Benaissa showed that chemical treatment by inorganic acids also caused changes in sorption capacity of sorbents based on chitin for Cd²⁺ ions [32].

Conclusions

Sewage sludge from municipal WWTP can be considered removable material for potential toxic metal sorption from liquid wastes. Data presented in our paper confirm the sorption capacity of dried anaerobic sludge for Co^{2+} ions up to 175 µmol per g of d.w. We found out that the effect of methylation by formaldehyde caused insignificant change in sorption capacity of sludge. On the other hand, esterification of carboxyl groups by methanol and modification of sludge surface by hydrochloric acid caused significant decrease in sorption capacity of sorbent (more than 90%). ⁶⁰Co gamma spectrometry and FT-IR analysis established the crucial role of carboxyl groups of anaerobic sludge in the sorption and hydroxyl groups of anaerobic sludge in the sorption process of Co^{2+} ions.

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