**Original Research** 

# Highly Selective and Efficient Porous Cu-Sn Bimetallic Electrocatalyst for CO<sub>2</sub> Reduction to Formate

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#### Abstract

In the current study, a simple chemical reduction method to synthesize bimetallic nanocatalyst of  $CuSn(OH)_6$  has been reported. The morphology, composition, size and electrochemical activity of the nanocatalyst have been investigated. The nanocatalyst exhibits porous/sponge-like morphology. The linear sweep voltammetry and chronoamperometry were employed to measure the current density/ current response. The synthesized catalyst was used for electrochemical reduction of  $CO_2$  to formate. The electrocatalytic results confirmed higher faradaic efficiency (FE), high and long term stable current density and lower Tafel slope for the synthesized nanocatalyst. The maximum obtained FE on bimetallic electrocatalyst for the only liquid product (formate) was nearly 83%. The improved electrocatalytic activity confirms synergistic effect between Cu and Sn as nanocatalyst that efficiently contributed towards the conversion of  $CO_2$  to formate. Therefore,  $CuSn(OH)_6$  nanocatalyst can be prepared by a simple and cost-effective method that can be further used for efficient and selective reduction of  $CO_2$ .

**Keywords**: bimetallic nanoparticles, CO<sub>2</sub> reduction, electrocatalyst, formate, porous catalyst, Faradaic efficiency

#### Introduction

Carbon dioxide  $(CO_2)$  is a ubiquitous and necessary molecule to sustain life on Earth. The concentration

of  $CO_2$  in the atmosphere is increasing day by day due to the burning of fossil fuels for industries and human activities [1]. The concentration of  $CO_2$  in the atmosphere has surpassed the level of 400 ppm in human history [2-4]. Such massive emission of  $CO_2$ in the atmosphere has caused air pollution and the greenhouse effect [5, 6]. To rectify the adverse effects of atmospheric  $CO_2$  and to reduce its level, several methods

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such as chemical reduction, electrochemical reduction, and photochemical reduction are usually employed. Reports revealed that electrochemical reduction is best among all the techniques, as it is eco-friendly and easy to establish [7-9]. Being linear molecule, CO<sub>2</sub> molecule is thermodynamically stable [10-12] having high activation overpotential that results in slow reaction kinetics [11, 13, 14] for its reduction reaction. The lereduction of CO<sub>2</sub> to CO<sub>2</sub><sup>--</sup> requires high overpotential i.e.  $E^{\circ} = -1.90$  V vs Standard Hydrogen Electrode at pH 7 [15]. This high overpotential may be due to the change in geometry of CO<sub>2</sub> from a linear molecule to a bent molecule [16]. In addition, low faradaic efficiency (FE), poor product selectivity [17], and competitive side reaction like hydrogen evolution reaction significantly lowers the CO<sub>2</sub> reduction products [13, 18].

Electroreduction of  $CO_2$  may yield variety of products and formate is one of the organic molecules produced during  $CO_2$  reduction [19, 20]. Formate is a simple, stable, nontoxic liquid and natural organic molecule [11, 21] that is used in dyes, leather, pesticides, silicones, and pharmaceutical industries. It is also used for the protection of crops, deicing of craft, in fuel cell and as an intermediate in many chemical processes [5, 11]. In order to convert  $CO_2$  to formate at low activation overpotential with high FE, an efficient, stable and product selective electrocatalyst is still needed.

Catalyst and electrode material contributes significantly to determining the overpotential, FE, and nature of the product in CO<sub>2</sub> reduction [22, 23]. Hori et al. reported that Pb, In, Cd, Tl, Bi, and Sn have been reported as efficient catalyst for formate production but require high negative potential [24-27] while Cu is famous for hydrocarbons [13, 28]. Some of the tested metals (Pb, Hg, Cd, In) are not preferred due to high cost and toxicity issues [29]. Copper expresses excellent behavior for electrochemical conversion of CO<sub>2</sub> to a variety of chemicals, but its selectivity is low [30]. However, Sn-based catalysts are good candidates for formate production because they are cost effective, selective and ecofriendly [11, 31, 32]. The catalytic activity and product selectivity can be improved by changing the catalyst or by changing the morphology of the catalyst after alloying [13, 33-35]. Therefore, the selectivity of Cu catalysts can be enhanced by the incorporation of secondary metal especially Sn, In, Ag and A1 [30].

In this manuscript, the preparation of Cu-Sn bimetallic nanocatalyst and their catalytic activity has been presented. The Cu-Sn bimetallic nanocatalyst was prepared by the chemical reduction method, which is cost-effective, time-saving and superficial. Synthesized alloy nanocatalyst was investigated for their catalytic activities for the conversion of  $CO_2$  to formate. Electrochemical study confirmed excellent stability, activity, current density, FE and formate selectivity. In addition, problems of product selectivity, high overpotential, low stability, current density and FE have been addressed successfully.

## **Material and Methods**

## Chemicals and Reagents

Salts of copper (II) chloride dihydrate (CuCl<sub>2</sub>.2H<sub>2</sub>O), sodium dodecyl sulfate (NaC<sub>12</sub>H<sub>25</sub>SO<sub>4</sub>), and tin(II) chloride dihydrate (SnCl<sub>2</sub>. 2H<sub>2</sub>O) and Isopropyl alcohol (IPA, C<sub>3</sub>H<sub>8</sub>O) were purchased from Unichem (China). The sodium borohydride (NaBH<sub>4</sub>, ≥96%,) was obtained from Sigma Aldrich. Food grade carbon dioxide (CO<sub>2</sub>, 99.999%) was obtained from the local market.

## Preparation of CuSn(OH)<sub>6</sub> Catalyst

of copper-tin The nanocatalyst hydroxide  $(CuSn(OH)_{\ell})$  were prepared via the chemical reduction method. CuCl<sub>2</sub>. 2H<sub>2</sub>O and SnCl<sub>2</sub>. 2H<sub>2</sub>O were used as precursor salts. First, the weighed amount of 0.86 g CuCl<sub>2</sub>. 2H<sub>2</sub>O and 4.06 g NaC<sub>12</sub>H<sub>25</sub>SO<sub>4</sub> were dissolved in 50 mL of distilled water and then 50 mL of IPA was added. The prepared mixture was then shifted to a 250 mL three neck round bottom (RB) flask. The RB flask was placed in a water bath at 50°C under a constant stirring of 500 rpm for 1 h. Then 10 mL of 5 M aqueous NaBH, was added dropwise. After 20 min, 0.101 g of SnCl<sub>2</sub>. 2H<sub>2</sub>O was added in the above mixture and heated for 3 h. The stirring and temperature of the reaction contents were maintained throughout the experiment. Synthesized nanocatalyst was collected through centrifugation (4000 rpm) for half an hour and then washed many times with water to remove the surfactant or any other water-soluble impurity. After washing, the final product was then dried in an oven at 70°C for 24 h and calcined at 300°C for 1 h.

## Catalyst Characterization

The suspension of nanocatalyst was prepared in IPA through ultra-sonification for particle size analysis and UV- Visible spectroscopy. The size of the nanocatalyst was estimated with particle size analyzer based on the dynamic light scattering (DLS) technique. The absorption spectrum,  $\boldsymbol{\lambda}_{max}\!,$  and energy bandgap were calculated from UV-Visible spectroscopy data. X-ray diffraction (XRD) pattern was acquired with Cu-K $\alpha$  radiations ( $\lambda = 1.54059$  Å, scan range 15-60° with step 0.05, scan rate 0.5 degree/min) and used to verify the crystal structure of the sample with JCPDS powder diffraction database. The percent crystallinity, the lattice constant, and hkl value were calculated from XRD data. The crystallite size was calculated employing Debye Scherrer's equation. Scanning electron microscope (SEM) images were taken to observe the morphology of the nanocatalyst. The fluorine-doped tin oxide (FTO) substrate was coated with catalyst ink/ slurry (detail of ink formation and catalyst coating are given in the electrode fabrication) to get SEM images. The FTO substrates adhered to the sample holder with conductive double-sided carbon tape. Linear sweep voltammetry (LSV) and chronoamperometry (CA) were finalized to evaluate the electrocatalytic behavior (current density) and stability of the catalyst for CO<sub>2</sub>RR.

#### **Electrode Fabrication**

The working electrode was prepared on the FTO substrate (a conducting glass) with a dimension of  $1\times2$  cm<sup>2</sup>. First, the FTO was dipped in 20 mL of ethanolic saturated KOH at 60°C and the 1 A current was passed for 2 min to activate the substrate, then washed with deionized water and air-dried. The ink/slurry of the catalyst was prepared by taking 10 mg of CuSn(OH)<sub>6</sub> catalyst in 950 µL of IPA and 50 µl of 5 %wt Nafion solution and subjected to ultrasonication for 3 h. Then the 50 µL slurry was drop cast on the activated FTO substrate and left for overnight drying at ambient conditions. After drying it was used for the electrocatalytic measurements.

#### Electrocatalysis Evaluation

The Metrohm auto lab (BV PGSTAT302N) with a three-electrode system was used for the electrochemical measurements. The two electrode compartments (H type cell) were separated with proton exchange membrane Nafion NRE-212 Sigma Aldrich. This separation helps to prevent the re-oxidation of reduction products of CO<sub>2</sub>. The 0.1 M KHCO<sub>2</sub> was used as an electrolyte. The 35 mL of electrolyte was filled in each compartment (cathodic and anodic). The catholyte was fed and saturated with CO<sub>2</sub> for at least 1 h before the start of electroreduction. The FTO substrate, coated with catalyst was inserted into the cathodic compartment as a working electrode. The Ag/AgCl electrode, a reference electrode, was positioned in the catholyte with proximity to the working electrode and the Pt sheet, the counter electrode, was inserted in the anolyte. The LSV (potential window from 0 to -1V, scan rate of 50 mV/s) and CA (at a fixed voltage of 0.9 V for 9) were performed to measure the response of current. All the reported potentials are against Ag/AgCl electrode otherwise stated. The reduction current and concentration of products were used to measure the catalytic activity.

#### **Results and Discussion**

#### Characterization of Nanocatalyst

The UV spectrum was measured from 250 to 800 nm to evaluate the optical properties of the catalyst and the result is shown in Fig. 1. The UV spectrum shows a single absorption peak at 293 nm. The  $Cu_xO_y$  shows the maximum absorption at 258 nm and ~650 nm while the pure copper nanoparticles have been reported to exhibit maximum absorption at 570-582 nm [36, 37].

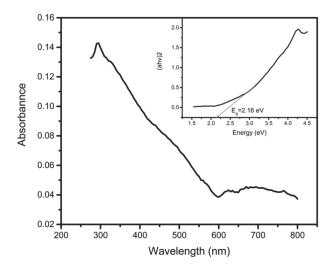


Fig. 1. UV-visible absorption spectra of  $\text{CuSn(OH)}_6$  (Inset Tauc plot).

The absorption maxima for SnO and  $Sn/SnO_{2-x}$  were reported in the range of 310-325 nm and 520-530 nm respectively [38]. The absence of characteristic peaks of Cu<sub>x</sub>O<sub>y</sub>, Cu, Sn, and Sn/SnO<sub>2-x</sub> rule out the presence of these individual nanoparticles. The absorption peak present in the IR region is at a lower wavelength from the nanoparticles cited in the literature, which indicates the nanocatalyst has blue-shifted and gives a strong response to the shorter wavelength that indicate smaller particle size of the nanocatalyst.

Dynamic light scattering (DLS) is a fast and easy technique for particle size distribution and to estimate the average size of the nanocatalyst [39]. We measured the average particle size by using particle size analyzer and the outcome is shown below in Fig. 2. The average estimated size of the nanocatalyst particles was found in the range of 10-22 nm. According to the literature, increase in catalytic activity may be observed due to smaller particle size as the surface area increases, as the size decreases. Thus, our catalyst may be efficient and highly active for  $CO_2$  reduction. The presence of a sharp peak indicates the nanocatalyst is monodispersed and of good quality.

The surface morphology of the catalyst was characterized by using SEM at different resolutions i.e. 2 and 5  $\mu$ m. Fig. 3 shows the surface of catalysts is sponge-like and porous with interconnected pores. The catalyst with a sponge-like morphology is beneficial and efficient because it provides high surface area which helps in the transportation of metal solvated ions as well as the maximum availability of the active sites of the catalyst. Moreover, the porous structure helps the electrochemical reduction of CO<sub>2</sub> by suppressing the hydrogen evolution reaction [40].

Powder X-Ray diffraction was used to check the crystalline structure, material composition, size of the crystallite and percent crystallinity. Fig. 4 presents the XRD pattern and unveils the highly crystalline nature (84%) of the as-prepared CuSn(OH)<sub>6</sub> catalyst.

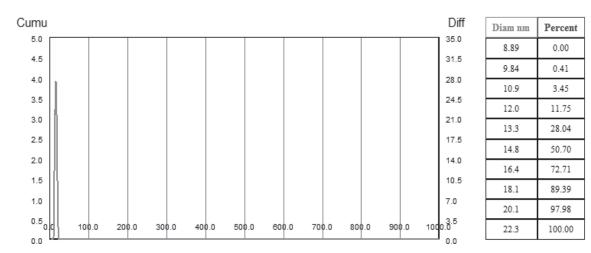


Fig. 2. Average size distribution of CuSn(OH)<sub>6</sub> nanocatalyst.

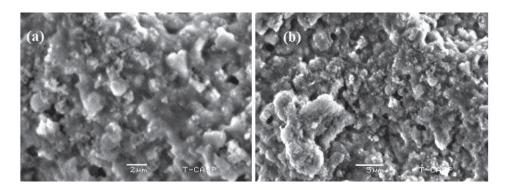


Fig. 3. SEM images of  $CuSn(OH)_6$  at different resolutions a) 2  $\mu$ m b) 5  $\mu$ m.

The diffraction peaks in the XRD pattern denotes the Bragg's reflections. The diffraction peaks at various positions (20) value  $18.76^{\circ}$ ,  $22.56^{\circ}$ ,  $31.94^{\circ}$ ,  $35.56^{\circ}$ ,  $37.81^{\circ}$ ,  $39.52^{\circ}$ ,  $42.29^{\circ}$ ,  $46.24^{\circ}$ ,  $52.65^{\circ}$ , and  $58.19^{\circ}$  correspond to the (111), (200), (220), (310), (311), (222), (321), (400), (420), (422) planes/facet of the crystalline phase. This crystalline phase is following JCPDS# 00-038-

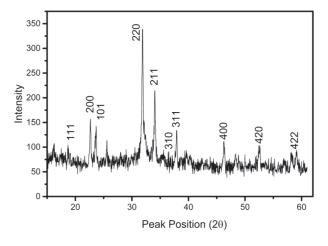


Fig. 4. P-XRD pattern of CuSn(OH)<sub>6</sub>

0394 (Crystal system: Cubic, a: 7.7350Å, Space group: Pn-3 m, Space group number: 224). The Debye Scherrer's equation was used to calculate the average crystallite size that was found in the range 16-22 nm. The particle size obtained from XRD is in agreement with the size obtained from DLS.

#### **Electrochemical Performance**

For electrochemical measurements of the catalyst, the H type cell was used. Fig. 5a) shows the LSV curves for the CuSn(OH)<sub>6</sub> catalyst in CO<sub>2</sub> saturated electrolyte (black) and air (grey). The onset potential and onset overpotential were calculated from the LSV curve and found to be -428 mV and -660 mV vs Ag/AgCl respectively. The catalyst with large onset overpotential (-660 mV) suppresses the HER that is the distinctive feature of the catalyst and is in agreement with its porous morphology. The suppression in HER favors the CO<sub>2</sub>RR otherwise current is consumed in HER instead of CO, reduction. This indicates our catalyst is more specific for CO<sub>2</sub>RR. A continuous increase in current density was observed beyond the onset potential. The maximum obtained current density was 24 mA/cm<sup>2</sup> at -1 V. The large current density is also compatible with the surface morphology of the catalyst. The small size

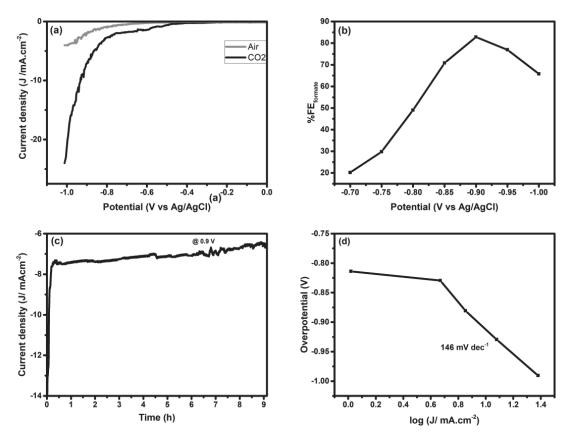


Fig. 5. a) LSV curve for  $CO_2$  saturated electrolyte (black) and without  $CO_2$  saturation (red). b) % FE for formate at different potentials c) Current response in chronoamperometry at 0.9 V vs Ag/AgCl d) Tafel plot for the formation of formate in 0.1M KHCO<sub>3</sub>

and the porous structure of the catalyst provide high surface area with a large number of active sites, which in turn improves the catalytic efficiency. The onset potential for air was high and the current density was lower as compared to the  $CO_2$  saturated electrolyte. The increase in current density in  $CO_2$  saturated electrolyte indicates the high activity of the catalyst for  $CO_2RR$ .

The  $CO_2$  electroreduction at different potentials (-0.7 to -1.0 V) was executed for the identification, quantification/characterization of products. Ion chromatography (Akta pure M1 model of FPLC equipped with ion exchange column) and UV visible spectroscopy was used for the identification and quantification of liquid product.

electrocatalytic CO<sub>2</sub> was The reduction of accomplished for 1 h at each potential (-0.7 to -1.0 V) for the product identification and FE calculation. The electrolyte sample was analyzed and results showed that the only liquid product under all potentials from CO, reduction was formate. The FEs for formate as a function of the potential is represented in Fig. 5b). A climb is observed in the  $FE_{Formate}$  with the increase in applied potential from -0.75 to -0.9 V. The maximum obtained FE was 82.8% at -0.9 V and a decrease in FE is observed beyond this potential. The highest FE for formate represents the collaboration between two metals and the presence of Cu with Sn modified the features of electroactive species.

For stability test, CA was done at -0.9 V for 9 h in  $CO_2$  saturated electrolyte. Fig. 5c) shows the stable cathodic current density during the chronoamperometric analysis which evidences the constancy of the catalyst. During bulk analysis, the average obtained FE<sub>formate</sub> was 78% which represents the high activity of the catalyst for long-term electrocatalysis. The stability test proves that the pre-synthesized CuSn(OH)<sub>6</sub> acts as a robust electrode and can be used in any device to reduce waste  $CO_2$  into formate.

The Tafel slope helps in the understanding of reaction kinetics/mechanism. The small value of the Tafel slope represents the high catalytic efficiency and the lower rate-limiting activation energy barrier. The Tafel plot was constructed to gain kinetic insights and the reaction pathway for CO<sub>2</sub> electroreduction to formate in the applied potential range of -0.7 to -1 V Fig. 5d). The obtained Tafel slope value (146 mV/dec) is following the mechanistic hypothesis which denotes the rate-determining step is the transfer of the first electron to the surface adsorbed CO<sub>2</sub> for the formation of radical anion (CO<sub>2</sub><sup>--</sup>) intermediate [41, 42]. Along with the reaction mechanism, the small slope also suggests that CuSn(OH)<sub>6</sub> exhibits the high reaction kinetics for CO<sub>2</sub> reaction.

The electrocatalytic activity, stability, and product selectivity of the catalyst was efficient and comparable with the literature i.e. hierarchical porous Cu foam at -1 V vs Ag/AgCl) [43] fibrous Cu at -1.1 V vs Ag/AgCl [44], porous SnO<sub>2</sub> wires at -0.8 V vs RHE [45], and 3D Sn foam on Sn film at -1.3 V vs RHE [46] have reduced CO<sub>2</sub> to formate with the FE of 43, 29, 80, and 90 % respectively. The selectivity, durability and electrocatalytic performance of the bimetallic catalyst for formate production were excellent.

#### Conclusions

The nanocatalyst  $\text{CuSn(OH)}_6$  was successfully synthesized by a chemical reduction method for the electrochemical reduction of CO<sub>2</sub> to formate. The catalyst exhibits the high FE of 82.8% at 0.9 V vs Ag/AgCl with stable current density (~7.6 mA cm<sup>-2</sup>) for 9 hours. The Tafel slope was only 146 mV/dec. The bimetallic catalyst exhibits admirable electrocatalytic activity towards CO<sub>2</sub>RR to formate in aqueous electrolyte. The great combination of high current density, stability, high FE and product selectivity makes the catalyst highly effective and efficient for CO<sub>2</sub>RR production from CO<sub>2</sub>.

#### **Conflict of Interest**

The authors declare no conflict of interest.

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